



Norsk olje & gass

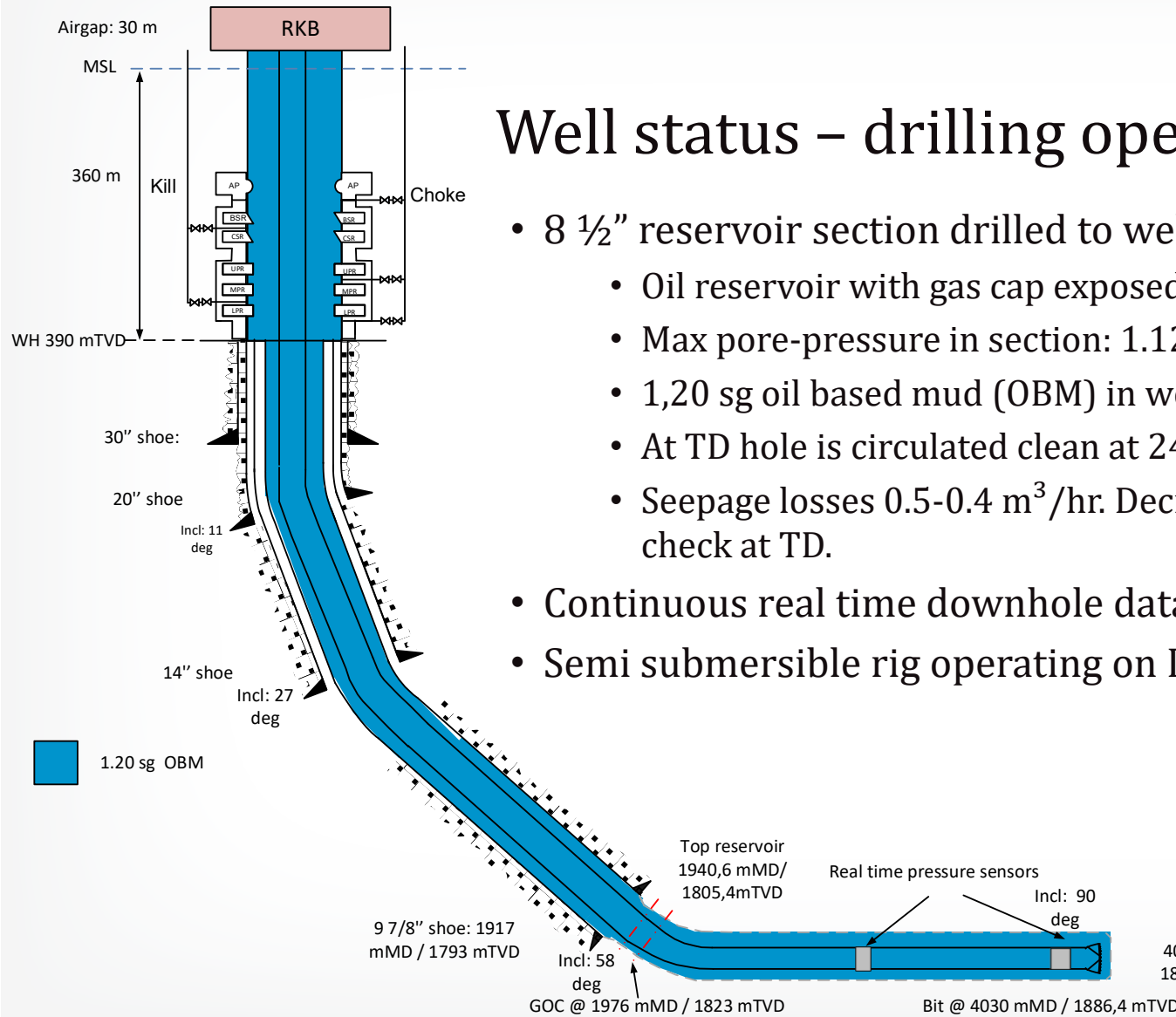
# "Sharing To Be Better"

No 22

Serious (yellow) well control incident -  
**Influx during displacement operation**

# Well status – drilling operations

- 8 1/2" reservoir section drilled to well TD at 4047 mMD
- Oil reservoir with gas cap exposed
- Max pore-pressure in section: 1.12 sg
- 1,20 sg oil based mud (OBM) in well
- At TD hole is circulated clean at 2400 lpm, ECD 1.53-1.54 sg.
- Seepage losses 0.5-0.4 m<sup>3</sup>/hr. Decreasing to 0.3 m<sup>3</sup>/hr after prolonged flow-check at TD.
- Continuous real time downhole data available (wired drill pipe)
- Semi submersible rig operating on Dynamic Positioning (DP)

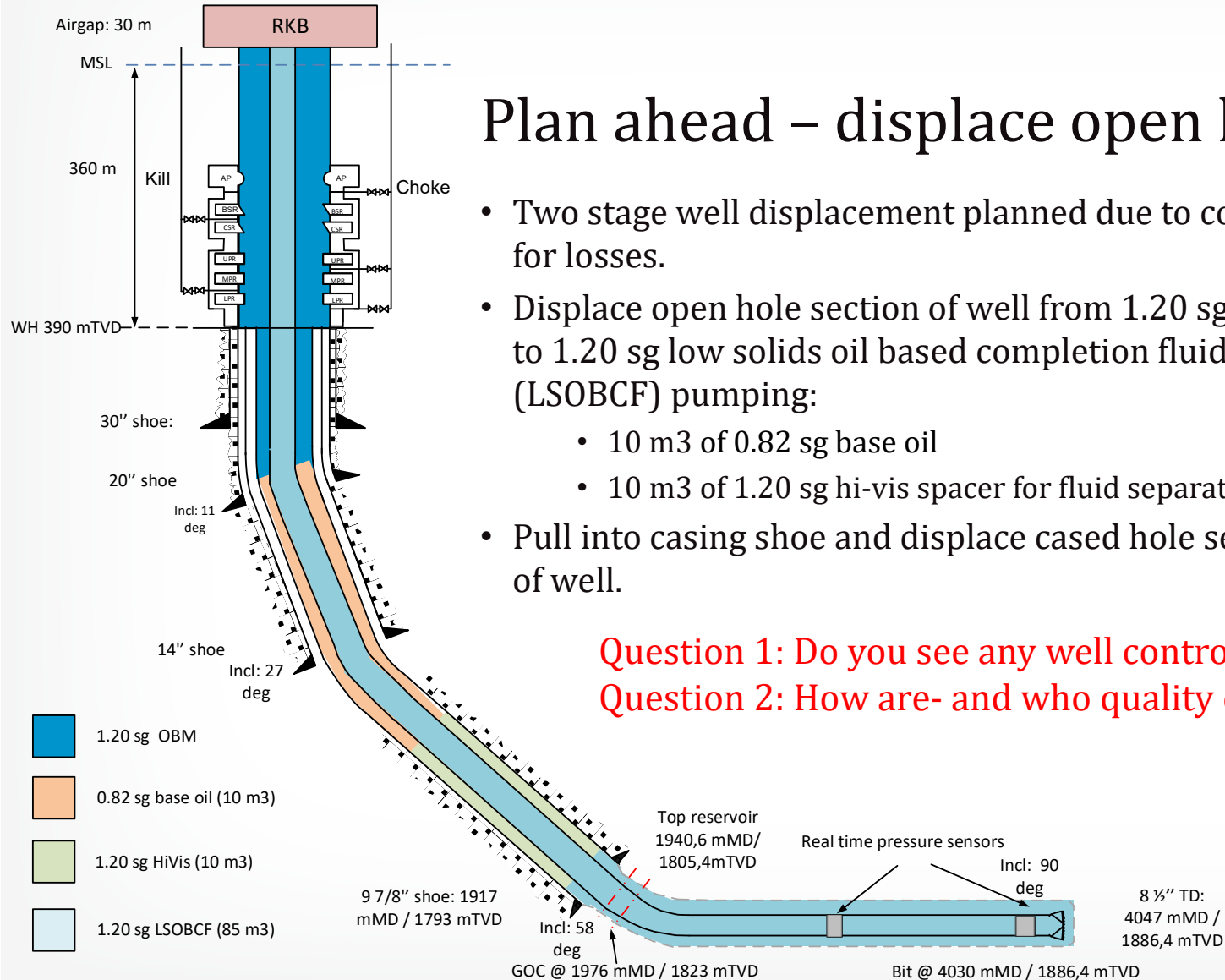


# Plan ahead – displace open hole section

- Two stage well displacement planned due to concern for losses.
- Displace open hole section of well from 1.20 sg OBM to 1.20 sg low solids oil based completion fluid (LSOBCF) pumping:
  - 10 m<sup>3</sup> of 0.82 sg base oil
  - 10 m<sup>3</sup> of 1.20 sg hi-vis spacer for fluid separation.
- Pull into casing shoe and displace cased hole section of well.

## Description from Detailed Operational Procedure (DOP)

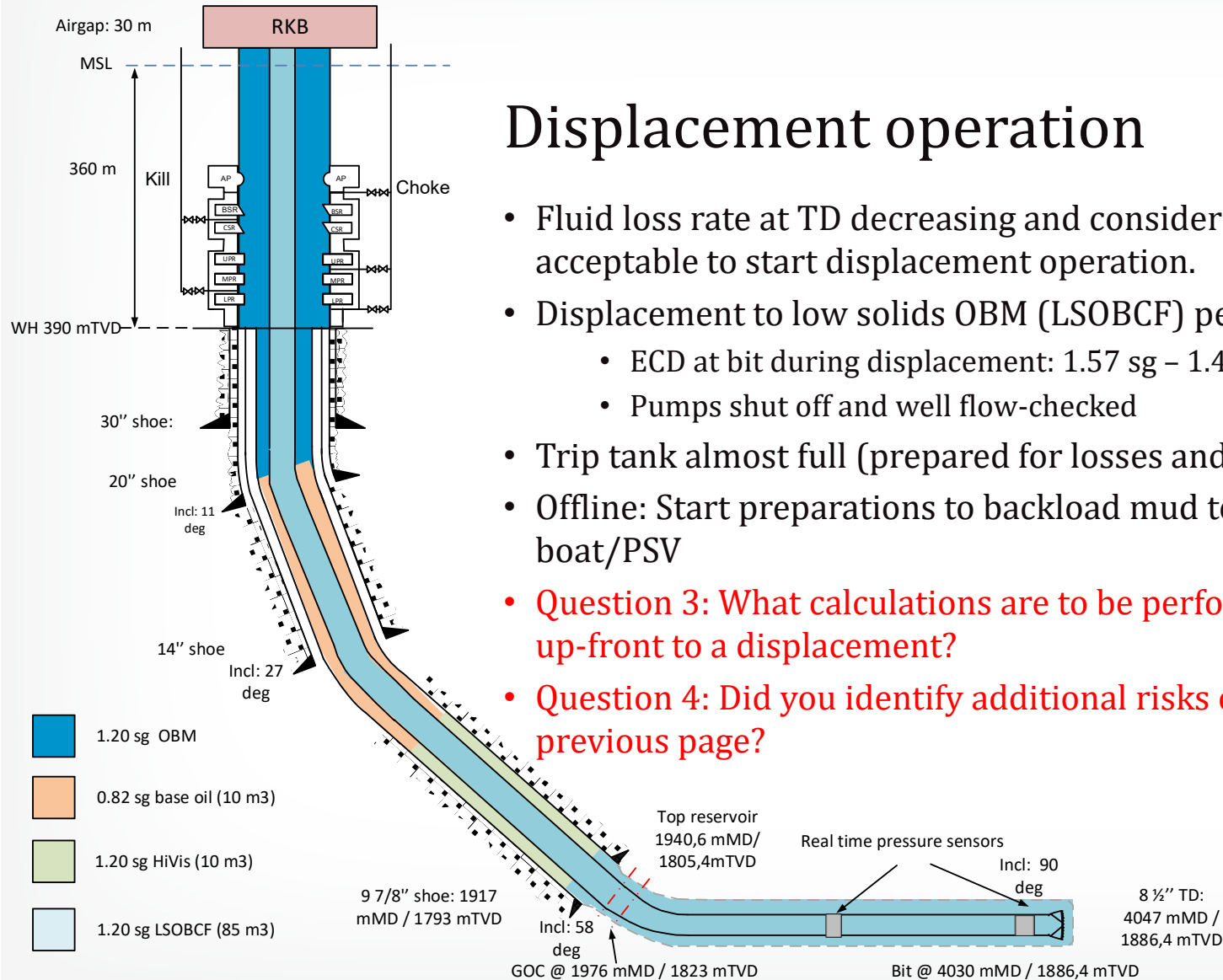
25. Displace OH to 1.20 sg LSOBCF according to mud engineer displacement program.
- Stay within max ECD confirmed by XLOT
  - Expect rapid increase in ECD
    - Careful as 1.20 sg LSOBCF enters open hole with bit on bottom
  - Pump total of 1x OH volume + 10 %



**Question 1: Do you see any well control risks with the planned operations?**  
**Question 2: How are- and who quality checks the displacement plans?**

# Displacement operation

- Fluid loss rate at TD decreasing and considered acceptable to start displacement operation.
- Displacement to low solids OBM (LSOBCF) performed
  - ECD at bit during displacement: 1.57 sg – 1.42 sg
  - Pumps shut off and well flow-checked
- Trip tank almost full (prepared for losses and POOH)
- Offline: Start preparations to backload mud to boat/PSV
- **Question 3: What calculations are to be performed up-front to a displacement?**
- **Question 4: Did you identify additional risks on previous page?**



## Communicated well control risks:

### HSE

- Losses
  - High ECD during drilling
  - High ECD during displacement to LSOBCF (rheology)

### Risk and mitigation:

- Losses
  - High ECD while exiting shoe
  - XLOT performed

### Risk and mitigation:

- Unable to stay within reservoir
  - reactively geosteer based on LWD
- Loss of data transfer
- Risk of losses
  1. Reduce MW, minimum 1.14 sg (no riser margin)
  2. If unable to cure losses, LCM is available on the rig

|                            |                              |   |   |
|----------------------------|------------------------------|---|---|
| 5.0-05<br>WI-PB<br>section | Losses while drilling 8 1/2" | • Drilling through fault<br>• High MW/ECD | HSE: • Loss of primary barrier<br><br>TC:<br>• Cement and redrill |
|----------------------------|------------------------------|---|---|

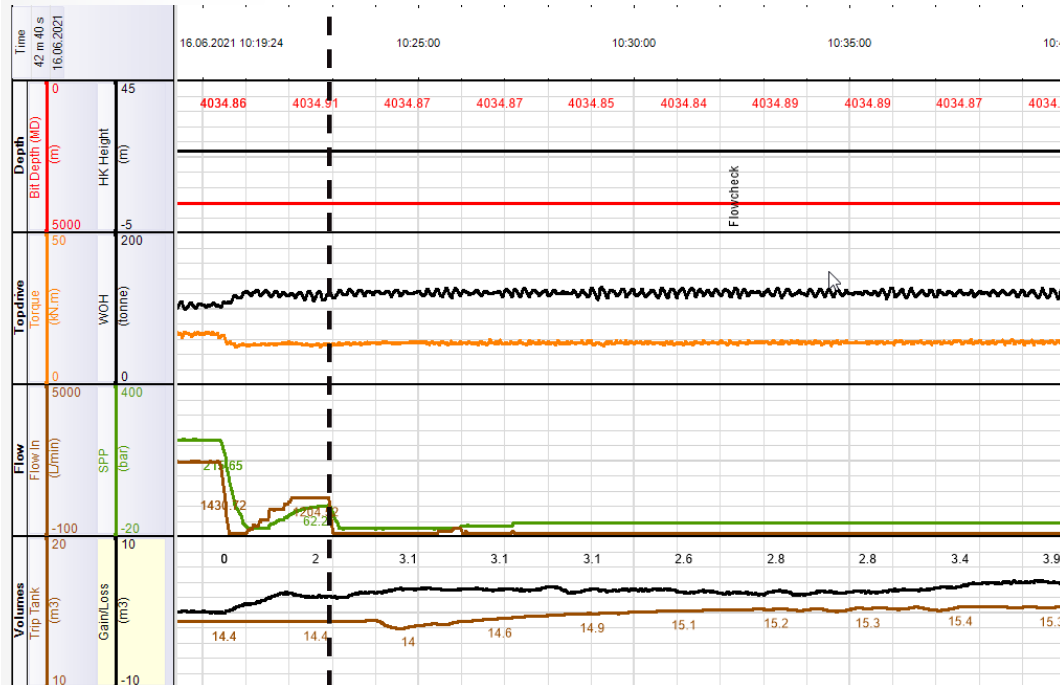


# Flow check after displacement 1/4

10:23 Pump shut-off – line over to TT.

10:23 - 10:30  
Flow back due to u-tube pressure

10:30 – 10:40  
Flow-checking well



The theoretical backflow due to u-tube pressure is 2.2 m3 (not known/calculated prior to flow-check by crew).

Be aware that the trip tank was not lined up immediately.

- Question 5: Is the flowback due to u-tube as expected?
- Question 6: Good flow-check or would you have extended it?

# Flow check after displacement 2/4

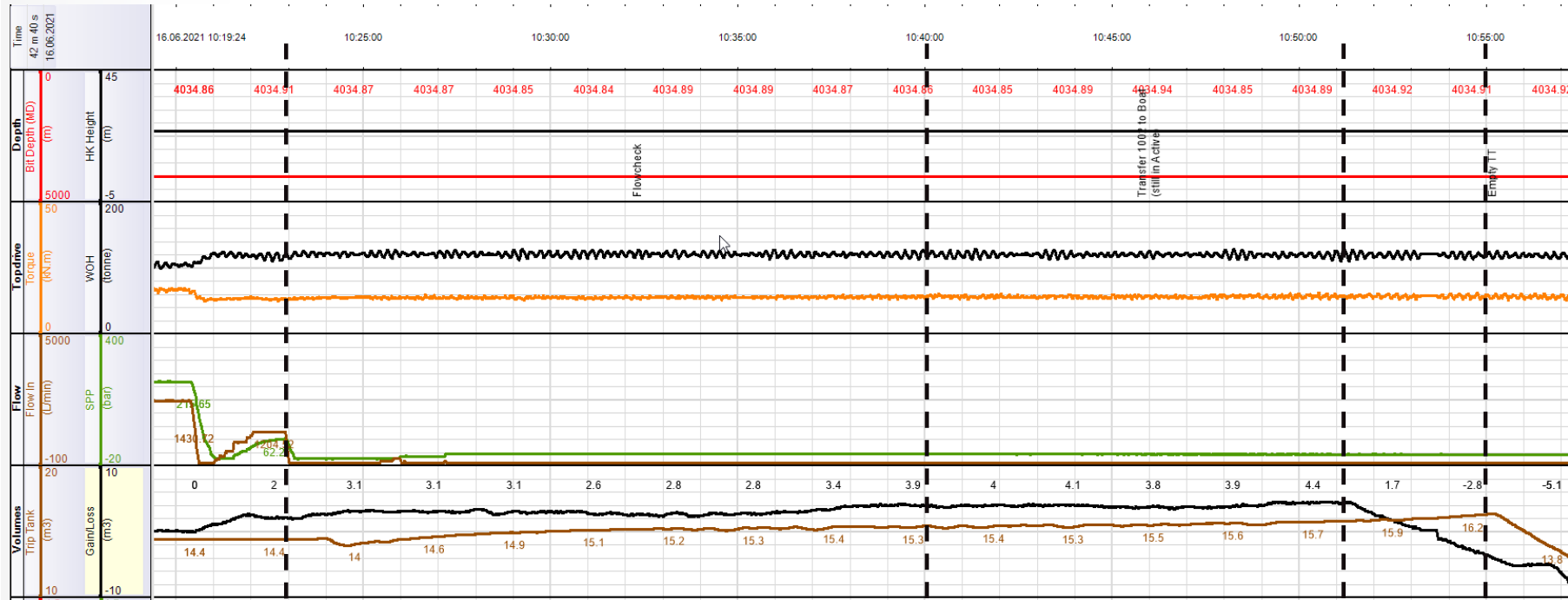
10:23 Pump shut-off – line over to TT.

10:23 - 10:30  
Flow back due to u-tube pressure

10:30 – 10:40  
Flow-checking well

10:51: Start off-load mud to boat / PSV

10:55: Decision to empty trip tank as it was close to full



- Question 7: What would you do if trip-tank was close to full in this scenario?
  - Empty TT, line over to 2<sup>nd</sup> TT (if available) or other?
- Question 8: What improvements to volume control do you see during the flow-check?



# Flow check after displacement 3/4

10:23 Pump shut-off – line over to TT.

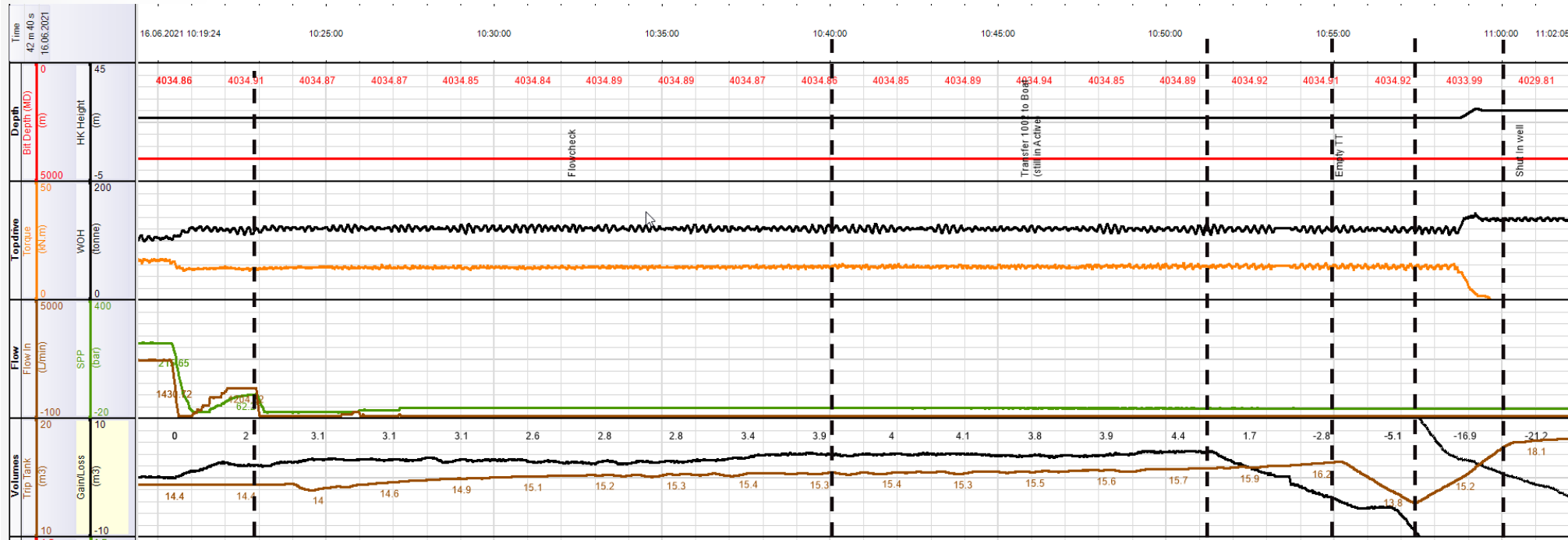
10:23 - 10:30  
Flow back due to u-tube pressure

10:30 – 10:40  
Flow-checking well

10:51: Start off-load mud to boat / PSV.

10:55: Need to empty trip tank as it is close to full

10:57: Back on trip-tank  
11:00: Well shut-in on annular



- Prior to start emptying the trip tank the flowback from well was ~ 135 liters/min.
  - After spending just over 2 minutes to empty TT, the flowback rate had increased to 2100 liters/min.
- **Question 9: What has happened?**

# Flow check after displacement 4/4

10:23 Pump shut-off – line over to TT.

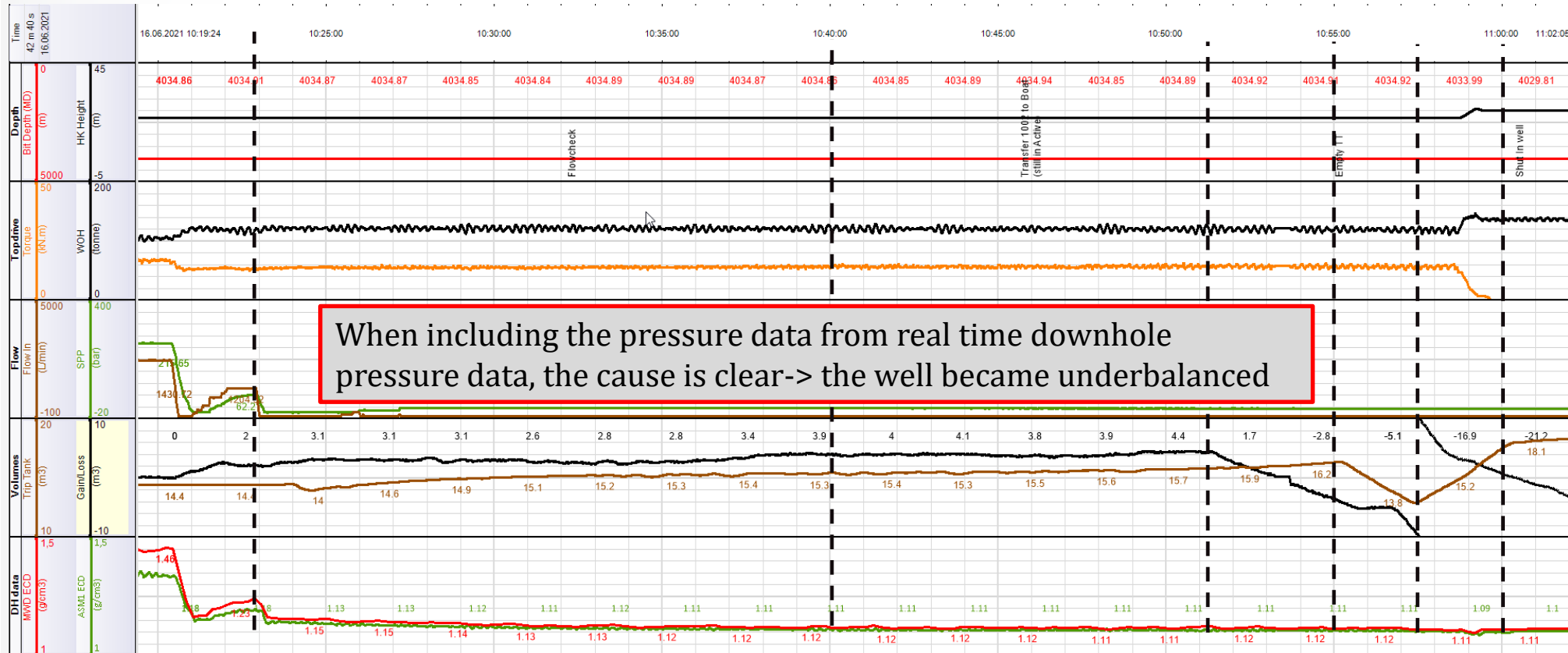
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When including the pressure data from real time downhole pressure data, the cause is clear -> the well became underbalanced

Pore pressure 1,12 sg

- Question 10: How do you ensure that all available data from the well are being used?
- Question 11: How to avoid becoming complacent towards sufficient overbalance in upcoming plans?

# Kick behaviour 1/2

• Question 12: How much safety margin/time left to shut-in well before hydrocarbons could have been above BOP and inside marine riser?

- Measured kick-size: 8,7 m<sup>3</sup>
- Annular volume from top reservoir to BOP: 30 m<sup>3</sup>

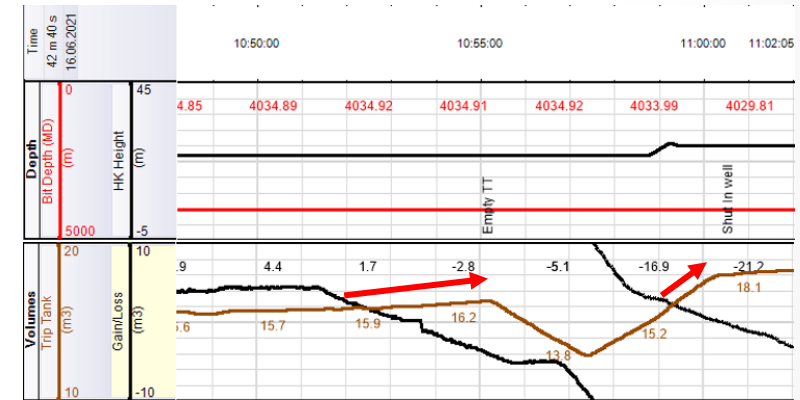
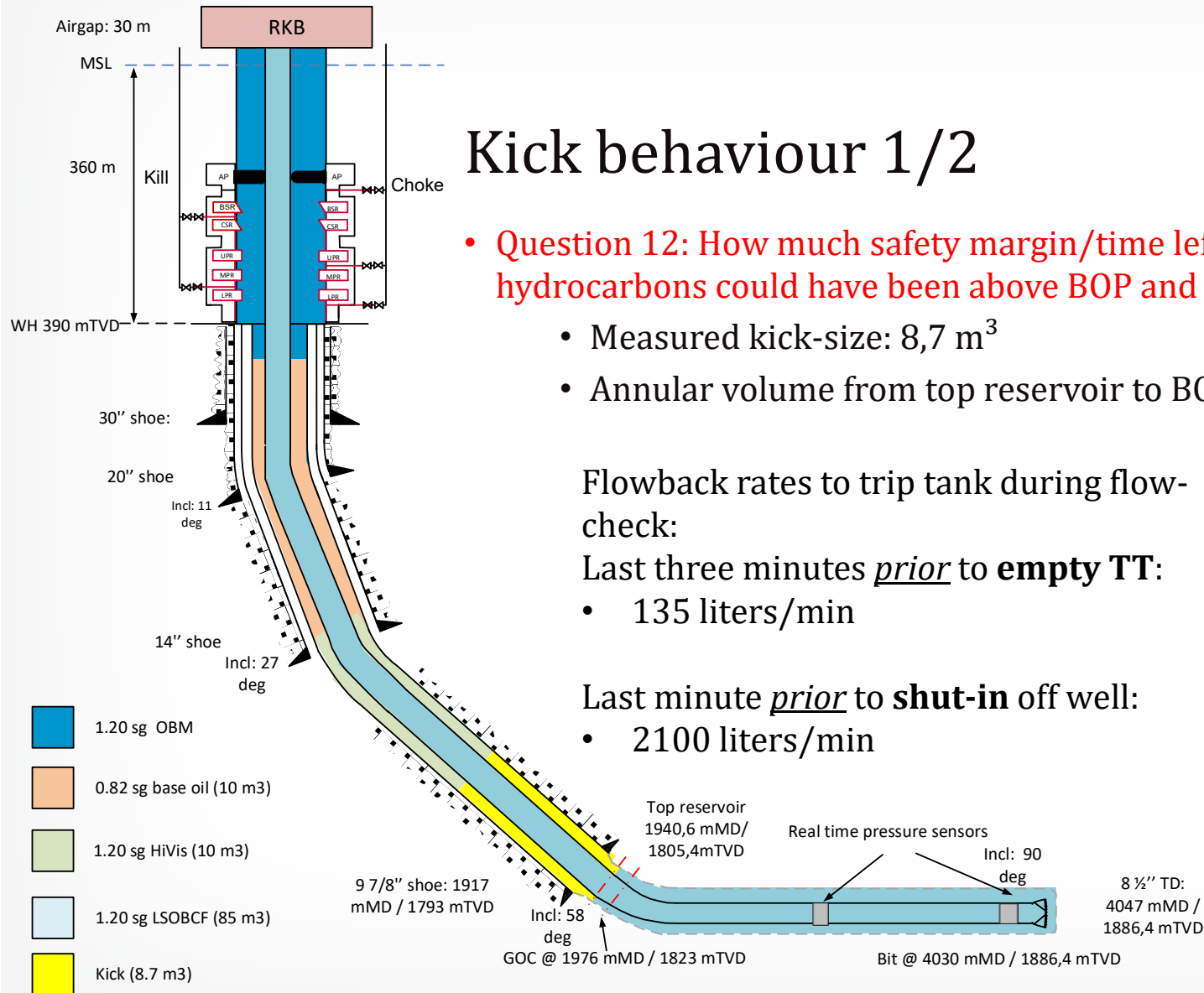
Flowback rates to trip tank during flow-check:

Last three minutes *prior* to **empty TT**:

- 135 liters/min

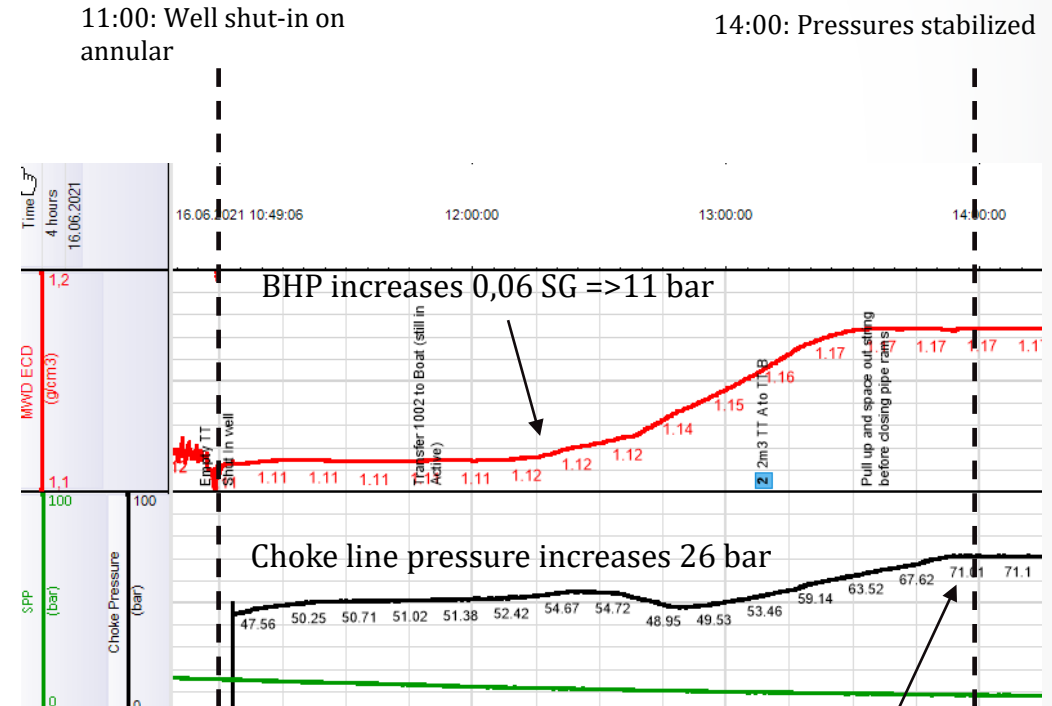
Last minute *prior* to **shut-in** off well:

- 2100 liters/min



## Kick behaviour 2/2

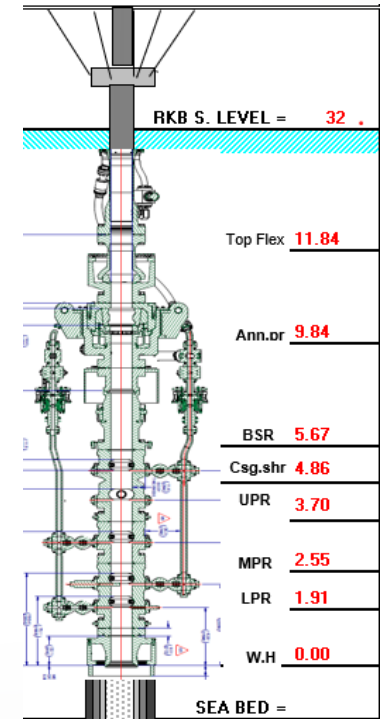
- Based on last observed rate of influx the safety margin for hydrocarbons above BOP was “maximum” 10 minutes, probably lower due to increasing kick-intensity.
- Question 13: Why do the BHP and choke/kill line pressures increase before stabilizing ~3 hrs after well was shut-in?**
  - Shut-in casing pressure: 45 bar
  - MAASP: 114 bar (w/1.20 sg mud)
- Question 14: Can you estimate the density of the influx?**
  - Choke/kill line length: 390 m,
  - Total volume in kill/choke line 5 m<sup>3</sup>, i.e. less than kick-volume.



Stabilized pressure at choke/kill: 71 bar  
 Stabilized pressure at wellhead: 78 bar

# Space out considerations

- At initial shut-in, the space-out of drill pipe tool joint was positioned for successful seal with annular preventer.
- When evaluating contingency plans it was identified that the tool joint was located 0,5 m above casing shear ram.
  - 5 7/8" tool joint not available/included in BOP shear-matrix
  - Indications of it being shearable when compared to similar OD tool joints.
- **Question 15: Would you proceed with the kill operation with this knowledge/space out?**



# Normalisation and handling the influx

- Large volume of gas kick taken into well.
  - Gas continued to migrate up well and up choke/kill lines after well shut-in.
  - Based on differences in surface kill/choke and subsea wellhead pressures the calculated influx-density is 0.18 sg EMW.
- Drillers method 1<sup>st</sup> circulation chosen to circulate the influx out of well
  - It was decided to strip up pipe to increase safety distance from tool joint to casing shear ram prior to kill operation, but this improvement was done 5 hrs after shut-in.
  - Choke operator used the surface choke pressure reading as primary gauge when circulating (as per normal procedures).
  - Real time downhole pressure data was monitored and made available to choke operator as supporting data.
  - **Question 16: How would you have utilized the real time downhole data when circulating out a kick?**
- Onshore well control response team mobilized to support offshore operations.
  - 24 hrs rotation established.

# Learning and recommendations

## **Risk management, Management of Change (MoC) and organizational factors:**

- Ensure proper QA/QC and compliance with MoC process.
  - Introduction of base oil was not part of Design of Service, unknown to key leading personnel and not discussed in Detailed Operational procedure (DOP) review.
- Include volumes and specify densities to be pumped in DOP.

## **Team and human factors:**

- All communicated and experienced risks was related to losses. Potential information bias resulting in delaying the shut-in of the well -> lower threshold for shutting in well.
- Enable crew to utilize downhole pressure data when available.
  - Clarify the responsibilities and increase awareness of wired drill pipe data to strengthen operational barrier elements.

## **Well control**

- Always calculate flow-back from u-tube and avoid flow-checking on full trip tank.
- Space out considerations